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Process Dynamics & Control By Dale E. Seborg, Thomas F. Edgar, and Duncan A. Mellichamp PART ONE: INTRODUCTION TO PROCESS CONTROL 1. Introduction to Process Control 1.1 Representative Process Control Problems 1.2 Illustrative Example 1.3 Classification of Process Control Strategies 1.4 A More Complicated Example--A Distillation Column

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Process temperature response for a step input b) The overshoot can be obtained from Eq. 5-52 or Fig. 5.11. From Figure 5.11 we see that OS = 0.05 for $\zeta = 0.7$. This means that maximum temperature is $T_{max} = 70 + (18)(1.05) = 70 + 18.9 = 88.9^\circ$ From Fig S5.15 we obtain a more accurate value.

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Process output for a ramp input 7-14 We know the response will come from product of $G(s)$ and $X_{\text{ramp}} = B/s^2$
KB Then $Y(s) = \frac{B}{s^2} \frac{K}{s + 2\zeta\omega_n s + \omega_n^2}$ From the ramp response of a first-order system we know that
the response will asymptotically approach a straight line with slope = KB.

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manipulated variable to maintain the process variable at a desired Set Point. A corollary to the definition of
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process control. 11.1 Introduction Some reasons for considering a system's dynamics and obtaining dynamic models are: 1. To describe the time behavior of a batch process. 2. To describe the transient response of a continuous process (e.g., dynamic change from one steady state to another). 3.

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